

# Temperature-Programmed Desorption as a Tool for Kinetic Analysis of NH<sub>3</sub> Decomposition on Ru/Al<sub>2</sub>O<sub>3</sub> and Ru/CeO<sub>2</sub>

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**Background and motivation.** Green NH<sub>3</sub> emerged as a promising H<sub>2</sub> carrier for energy transition<sup>1</sup>. Among catalysts used for ammonia decomposition, Ru shows the higher activity<sup>2</sup>. In this work, Ru/CeO<sub>2</sub> and Ru/Al<sub>2</sub>O<sub>3</sub> catalysts were synthesized via traditional wet impregnation and tested with steady state and transient response methods. The study focused on assessing how the choice of support material influences the catalytic behaviour and reaction kinetics in NH<sub>3</sub> decomposition.

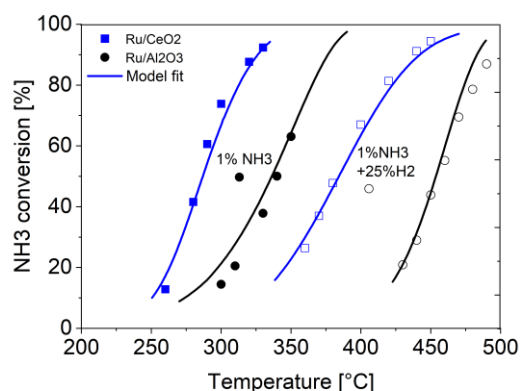
**Materials and methods.** Ru/Al<sub>2</sub>O<sub>3</sub> and Ru/CeO<sub>2</sub> catalysts were prepared by incipient wetness impregnation using Ru(NO)(NO<sub>3</sub>)<sub>3</sub> precursor, characterized by XRD, Raman, DRIFTS, CO chemisorption, and pre-treated with 1% H<sub>2</sub> flow in He from 50°C to 450°C before testing. NH<sub>3</sub> cracking was performed in micro-fixed bed unit, with diluted NH<sub>3</sub> in He. H<sub>2</sub> and N<sub>2</sub> cofeeding tests were performed. All tests were conducted at 20,000 NI/h/kgcat. The modelling analysis was based on 1D pseudo-homogeneous reactor model. Dynamic N<sub>2</sub>/H<sub>2</sub>/NH<sub>3</sub> adsorption/desorption experiments are now being performed to measure surface coverage evolution with temperature and support the kinetic investigation.

**Results and discussion.** Characterization results show high dispersion of Ru for both catalysts. As shown in Figure 1, Ru/CeO<sub>2</sub> catalysts outperformed Ru/Al<sub>2</sub>O<sub>3</sub>. The kinetic study suggests that NH<sub>3</sub> cracking over Ru/Al<sub>2</sub>O<sub>3</sub> is limited by NH<sub>3</sub> activation and H\* surface poisoning across the entire temperature range. By contrast, experiments involving Ru/CeO<sub>2</sub> catalysts are best explained by assuming that N\* desorption is rate-limiting at low temperatures, while NH<sub>3</sub> activation and H\* poisoning control the rate at higher temperatures. Preliminary results from dynamic experiments show that N\* species prevail below 300 °C, while the surface becomes H\*-rich at higher temperatures.

**Keywords:** ammonia cracking, ceria catalysts, temperature-programmed-desorption

## References

- [1] Triviño, M.L.T. et al., *Chem. Eng. J.* **2023**, 476, 146715.
- [2] Yamazaki, K. et al., *Appl. Catal. B* **2023**, 325, 122352.



**Figure 1.** Catalytic activity and kinetic model comparison for Ru/CeO<sub>2</sub> and Ru/Al<sub>2</sub>O<sub>3</sub>